

Amendments to the Specification:

On page 1, in the paragraph regarding the cross reference to related applications, please amend the paragraph as follows:

This application is a continuation of U.S. Application No. 09/129,911, filed August 6, 1998, now abandoned, which is a divisional of U.S. Application No. 08/655,735; filed May 30, 1996, now U.S. Patent No. 5,824,273.

On page 18, beginning on line 18 through page 19, line 1, please amend the paragraph as follows:

Moreover, valves 21, 22 and 23 are installed so as to controllably connect the inlet port for the reducing gas A of each reaction column 1 with the aforesaid first gas inlet line 11, second gas inlet line [[11]] 12 and regeneration gas outlet line 14, respectively. Similarly, valves 24, 25 and 26 are installed so as to controllably connect the outlet port for the reducing gas A of each reaction column 1 with refined gas outlet line 13, regeneration recycle gas inlet line 15 and reducing gas return line 16, respectively.

Beginning on page 44, please amend Abstract as follows:

~~This invention relates to a gas refining system wherein sulfur compounds contained in a high temperature and high pressure reducing gas obtained by the pressure gasification of coal or heavy oil or the like are adsorbed and removed in the form of a sulfide by an adsorbent, the adsorbent having the sulfide formed thereon is regenerated by roasting it with an oxygen-containing gas, and the regeneration gas containing sulfur dioxide formed by the roasting reaction is introduced into a reactor (50) where, by use of gas blowing means, the regeneration gas and an oxygen containing gas are blown into a calcium compound containing slurry fed to~~

the reactor (50), and thereby brought into gas-liquid contact with the slurry to effect the absorption of sulfur dioxide and the precipitation of gypsum within the reactor (50), characterized in that the gas refining system is provided with temperature control means for selectively controlling the temperature of the slurry within the reactor (50) so as to fall within at least a first temperature range which causes α -gypsum hemihydrate to precipitate or a second temperature range which causes gypsum dihydrate to precipitate. This invention is also characterized by the reactor (50) having a pressure vessel into which the regeneration gas can be blown under at least a pressure higher than atmospheric pressure, and by the gas blowing means comprising a stirring rod (63) disposed in the lower part of the reactor (50) so as to be horizontally rotatable, and at least a gas supply pipe (64) disposed integrally with the stirring rod (63) for injecting the regeneration gas and the oxygen-containing gas in the vicinity of the stirring rod (63).

A gas refining method for adsorbing a reducing gas obtained by pressure gasification of coal or oil comprises introducing a reducing gas stream into an adsorbing and removing zone where it contacts an adsorbent. Sulfur-containing compounds are adsorbed onto the adsorbent and a first oxygen-containing gas stream is introduced into the adsorbing and removing zone in order to form a regeneration gas containing sulfur dioxide. The regeneration gas is contacted with a second oxygen-containing stream and a calcium-containing liquid slurry to effect absorption of sulfur dioxide by the slurry and precipitation of a gypsum compound. The temperature of the slurry is varied to cause selective precipitation of α -gypsum hemihydrate or gypsum dihydrate.

Amendments to the Drawings:

The Examiner has objected to Figure 3 due to a typographical error. Applicants submit herewith, in the attached appendix, a new formal drawing of Fig. 3 wherein "E" has been replaced with --F--. In light of the foregoing, Applicants respectfully request reconsideration and withdrawal of the objection.